

# R.A.C

## Introduction

Temp.

$$\frac{C}{5} = \frac{F-32}{9}$$

$$9C = 5(F-32)$$

$$9C = 5(C-32) = 5C-160$$

$$4C = -160, C = -40$$

$$-40^{\circ}C = -40^{\circ}F$$

$$^{\circ}K = ^{\circ}C + 273, \quad ^{\circ}R = ^{\circ}F + 460$$

Absolute Zero =  $-273^{\circ}C$

Pr

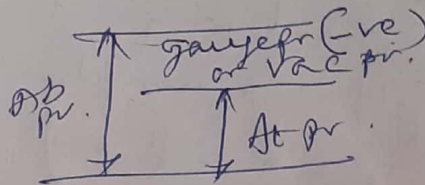
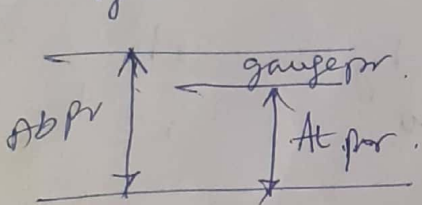
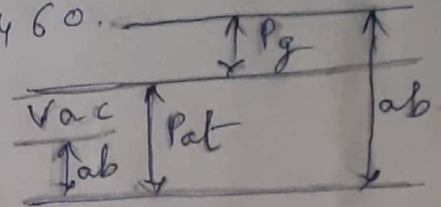
$$A_b Pr = A_t Pr + \text{gauge Pr}$$

For -ve values of Pr.

$$A_b Pr = A_t Pr - \text{vac. Pr}$$

$$P_{ab} + P_{vac} = P_a$$

$$P_{at} (-P_{vac}) = P_{ab}$$



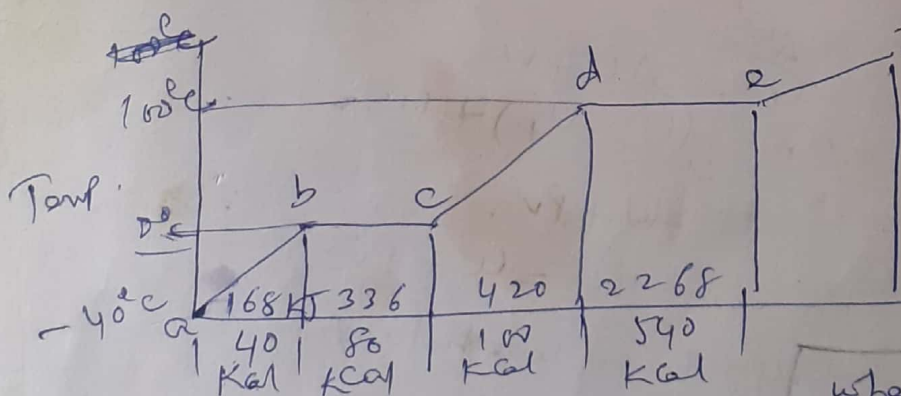
ex 1.2, 1.3. Khuram.

Heat

$$Q = mc_p (\Delta T)$$

Total heat

$$\text{Total ht} = \text{Sensible ht} + \text{Latent ht}$$



ab  $\rightarrow$  SH of ice

bc  $\rightarrow$  latent ht of fusion

cd  $\rightarrow$  SH of vaporization

de  $\rightarrow$  LH of vaporization

ef  $\rightarrow$  super heat

$$Pr = 1.032 \text{ bar}$$

when 1 kg of ice changes into water at const temp of  $0^{\circ}C$ , 334.5 KJ are absorbed from surroundings.

## Vapours

- ① Sat liq  $\rightarrow$  The heat of liq reaches its max value when the liq is in saturation condition exists.

Dry Saturated vapour:  
The vapour given off by boiling liq is at the same temp as the liq and the vapour is called the saturated vap. (dry vap).

mixture of vap + ~~liq~~ sat liq = wet sat vap.

$$\text{dryness fraction of wet sat vap} = \frac{M}{M+m}$$

(x)

M = wt of dry vap, m = entrained liq particles.

## 1st law

$$E_1 + Q = E_2$$

If work is ~~dev~~ developed by the system

$$Q = (E_2 - E_1) + W$$

Internal energy  $U = E - KE - PE$

Stored energy  $E = U + KE + PE$

$$dE = dU + dKE + dPE$$

closed system  $dKE = 0, dPE = 0,$   
 $dE = dU$

~~$$Q = \Delta U + W$$~~

$$Q = (U_2 - U_1) + W$$

## enthalpy

$$H = U + Pv$$

per unit mass,  $h = u + Pv$

enthalpy is a useful property.

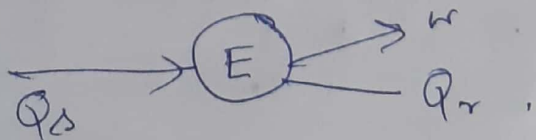
## Joule's law

~~$$Q = W J$$~~

$$Q = W J$$

$$J = \frac{Q}{W}$$

## 2nd law



entropy  $ds = \int \frac{dq}{T}$ ,  $w = \int_1^2 p dv$   
 $dq = T \cdot ds$ ,  $dw = p \cdot dv$

Refrn & 2nd law of Thermodynamics

low Temp to high Temp ,,

input of work is essential

Heat Tr . Conduction, Convection, radiation

Newton's law of cooling ,

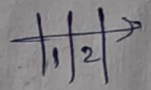
Heat Tr from hot body to cold body is directly proportional to surface area & diff in temp ,

Fourier's law of heat conduction

$$Q \propto KA \frac{dT}{dx} = \frac{KA(T_1 - T_2)}{Ax}$$

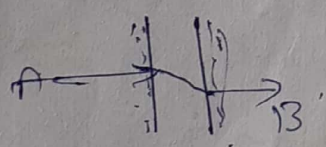
Composite wall .

- $x_1 =$  Thickness of Mat
- $K_1 =$  Thermal conductivity of Mat.
- $x_2 =$
- $K_2 =$



$$Q = \frac{A(T_1 - T_2)}{\frac{x_1}{K_1} + \frac{x_2}{K_2}} = \frac{A(T_1 - T_2)}{\sum \frac{x}{AK}}$$

overall heat Tr coefft  
(by conduction & convection)



$T_A$  &  $T_B =$  Temp of films.  
 $h_A$  &  $h_B =$  Coeffts of ht at films.

$U =$  overall ht

$$Q = UA \Delta T$$

Derivation

$$U = \frac{1}{\left(\frac{1}{h_A} + \frac{x}{K} + \frac{1}{h_B}\right)}$$

extended

$$U = \frac{1}{\frac{1}{h_A} + \frac{x_1}{K_1} + \frac{x_2}{K_2} + \frac{1}{h_B}}$$

Method of Refrig.

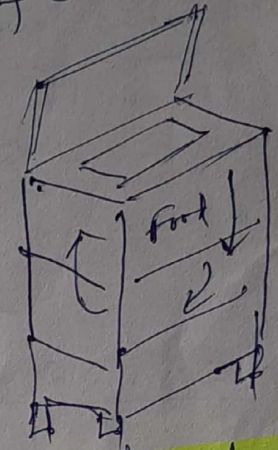
ASRE, American Society of Ref. Engrs  
 ASHRAE - American Society of Heating, Refrig. & Air Conditioning Engrs

ASRE

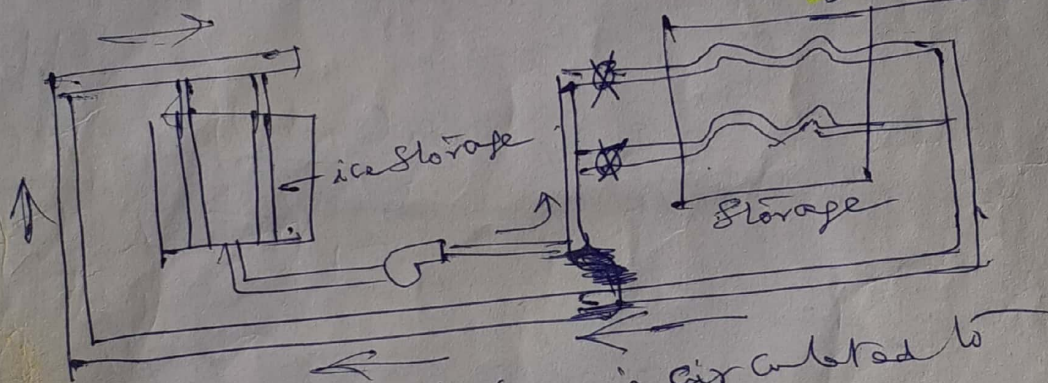
defines the Science of providing & maintaining temp below that of surrounding atmosphere.

1) ice Refrigerator.

Cold air goes down, hot air goes up. convection currents are developed. Food gets cooled.

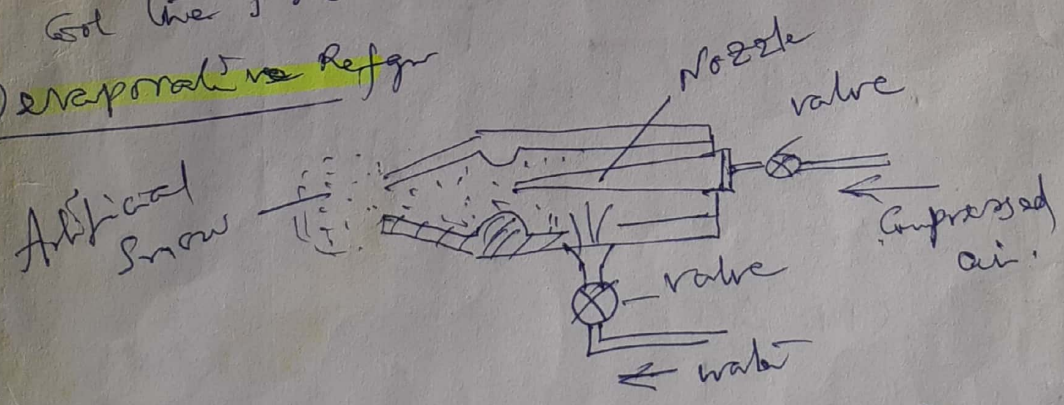


Direct System



Ice gets brine & brine is circulated to cool the products. (indirect Refrig.)

2) evaporative Refrig.



Heat is absorbed when a liq. evaporates, evaporation causes cooling. (ex:- sweat), desert bag.

Here - water goes out with air as tiny droplets. If outside air is near freezing, water droplets evaporate & ice is formed. Artificial Snow is formed. Snow can be made at 2°C

Unit of Refrig

$$\frac{2000 \text{ lb} \times 144 \text{ BTU/lb}}{24} = 12000 \text{ BTU/hr}$$

or ~~1000~~  $\frac{1000 \times 335 \text{ kJ}}{24 \text{ hr}}$  is 24 hr  
 $= \frac{1000 \times 335}{24 \times 60} = 232 \text{ kJ/min}$

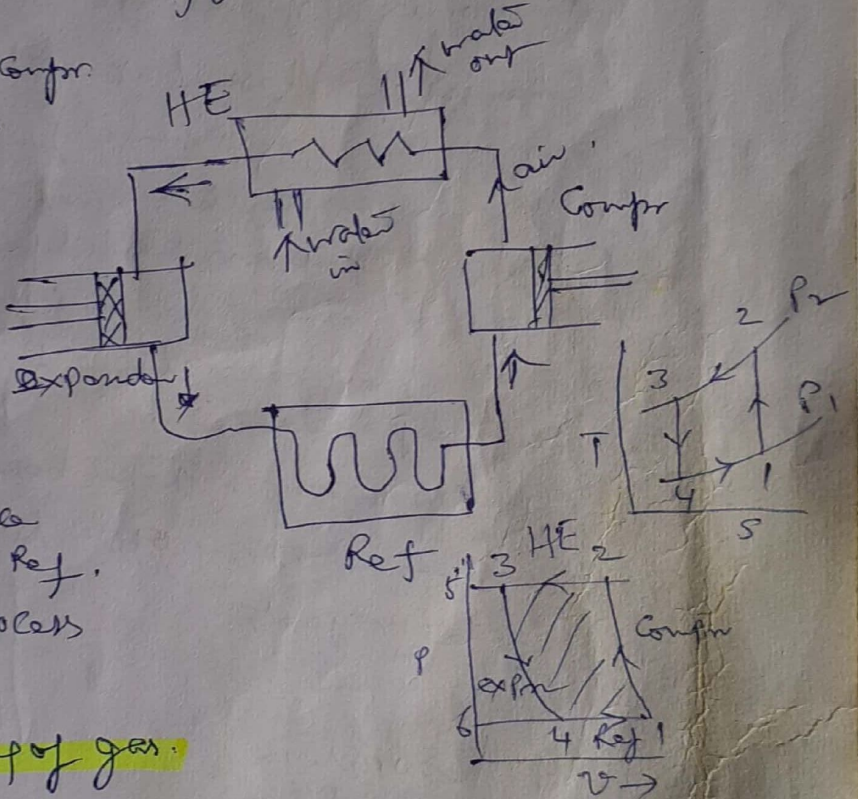
Taken as **210 kJ/min** or **3.5 kJ/s.**

2000 lbs  
 $= 909.1 \text{ kg}$   
 L.H. of ice =  $335 \text{ kJ/kg}$   
 Heat removed to  
 for 1 Billion Ton  
 of ice from  
 sea water to  
 sea ice  
 $\frac{909.1 \times 335}{24 \times 3600}$   
 $= 3.52 \text{ kJ/hr}$   
 $= 3.52 \text{ W}$

3) Refrigeration by expansion of air

Bell-Coleman air-refrig system.

- i) air is compressed in Compr.
- ii) High pr, High temp air is cooled in HE by water
- iii) expanded isentropically in expander till it reaches atmospheric pr. Cooling takes place
- iv) Cooled goes to Ref. gains heat and process repeats.



4) Ref by throttling of gas.

$$\mu = \left( \frac{\partial T}{\partial p} \right)_h \text{ at const enthalpy process}$$

$\mu =$  Joule Thomson coefficient,  $\mu$ -efficient.

$\mu = 0$  at inversion point.

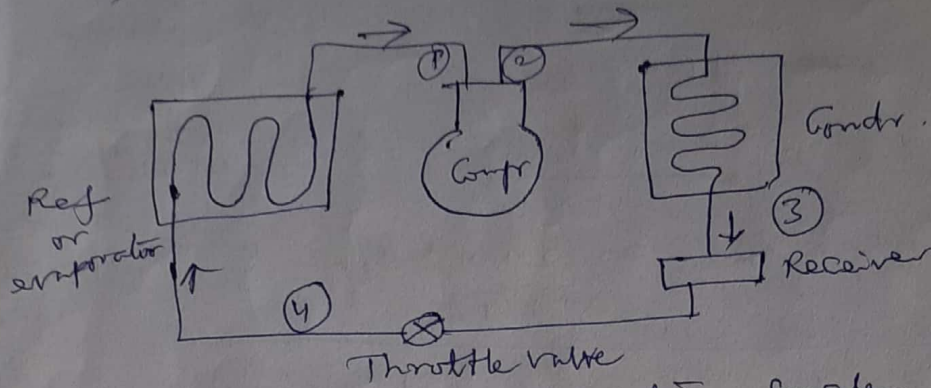
To reduce the temp after throttling  $\mu$  must be +ve.

~~By above method low temp cannot be obtained unless the original temp is low.~~

5) Vapor Refrigeration System

5/a) Vapor Compression Refrig System.

(8)



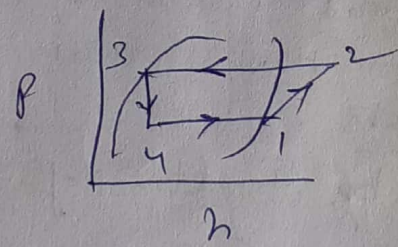
Refrigerants are used in this cycle  
Ammonia, Freons etc.

Change of phase takes place in this cycle  
In Air refriger no change of phase takes place  
vapor compr cycle is shown

- ① Refrig is compressed in Compr.
- ② Cooled in Cond'r ③ fills up in Receiver
- ④ expanded by throttling device (valve or capillary tube)
- ⑤ ~~Pr~~ Temp reduces.
- ⑥ goes to evap. Takes heat from products  
Becomes a vapor, goes to Compr

Cycle repeats

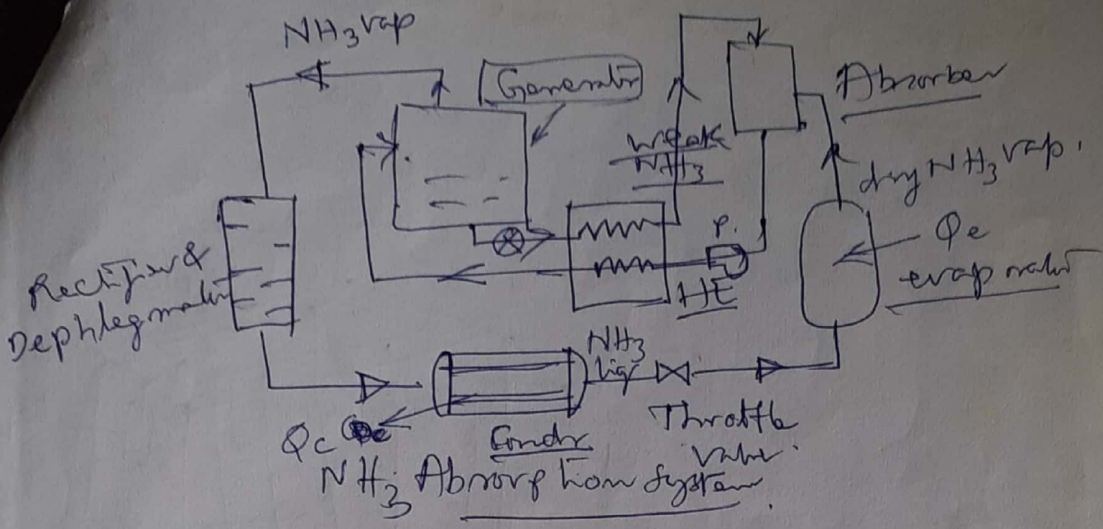
This is widely used.



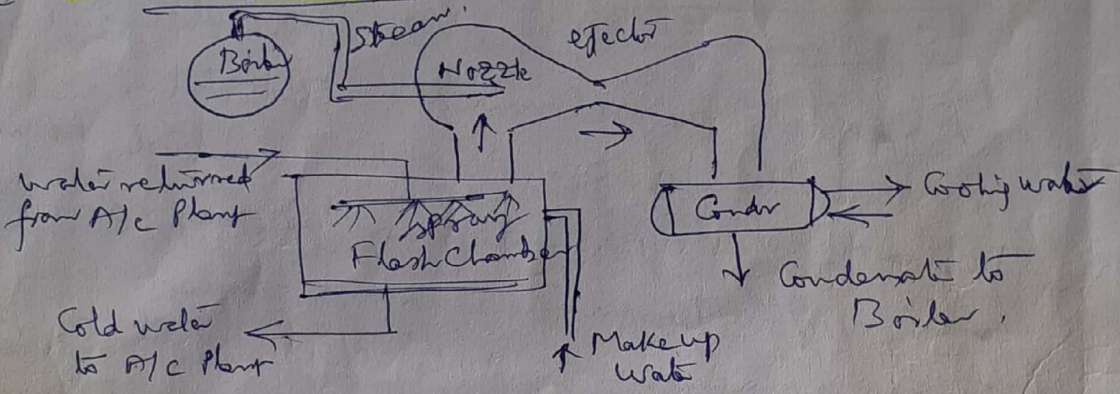
5/b) Vapor Absorption System.

In ammonia Absorption system water is the absorbent &  $\text{NH}_3$  is refrigerant.

From generator  $\text{NH}_3$  vapor goes to Cond'r,  $\text{NH}_3$  liq is formed, throttled and goes to evaporator, gains heat & the dry  $\text{NH}_3$  vap goes to Absorber. Here in absorber weak  $\text{NH}_3$  soln mixes with  $\text{NH}_3$  vap & becomes strong soln & goes to Generator. Cycle repeats.



6) Steam Jet Ref.



Steam Jet Refrig.

water boils at temps below 100°C, if the pressure on the surface of water is reduced below Atmospheric pressure. (Ex:- water boils at 6°C if the pressure on the surface is 5cm of water)

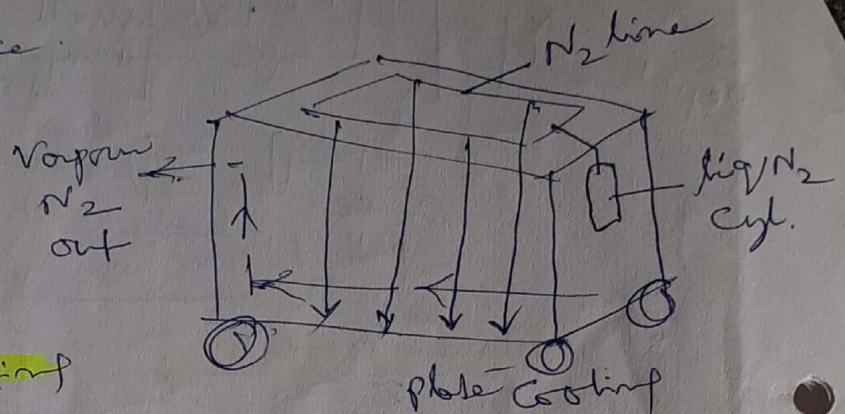
High pressure steam is expanded in the Nozzle. water vapour from flash chamber is entrained <sup>with</sup> the high velocity steam jet & is further compressed in the thermocompressor. & goes to condenser. The condensate goes to boiler.

The chilled water in evaporator is pumped to A/C plant and again returned back to the evaporator, and the cycle continues.

ex:- 100kg water, 1kg boiled in steam jet process.  
 99 kg is remaining water,  $\rightarrow \frac{2394 \text{ KJ}}{4.2 \times 99} = \Delta T = 5.7^\circ\text{C}$  fall in Temp.

## 7) Refrigeration by using liquid gases.

The use of liq  $N_2$ , liquid  $CO_2$  for cooling transportation vehicles is gaining importance.

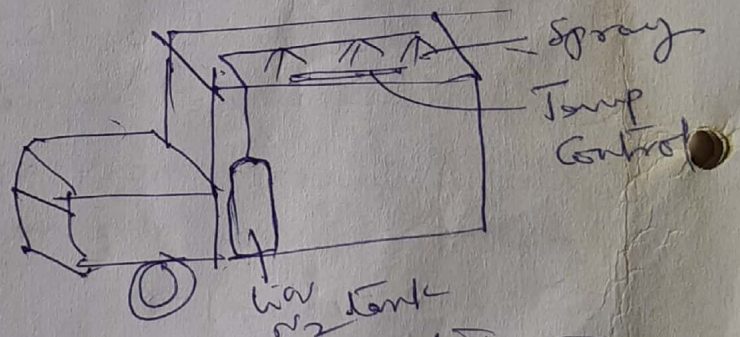


### a) Cold Plate Cooling System

liq  $N_2$  is passed into the cold plates. It is controlled by operating the control valves. liq  $N_2$  vapourises gaining heat from products.  $N_2$  vapour leaves the cargo space. There is no direct contact of  $N_2$  with cargo. Temps between  $-30^\circ C$  to  $20^\circ C$  are possible to attain.

### b) Spray Cooling.

In this liq  $N_2$  is directly sprayed into the refrigerated area.



Safety is more important in this. ( $N_2$  or  $CO_2$  can be used).

If liq  $N_2$  touches the human body, the part gets frozen.

### 8) Dry ice Refrigeration

Dry ice is solid  $CO_2$ . Sublimation Temp is  $-78^\circ C$ . It is used for frozen food. Slabs of dry ice are packed in between the food packets. This is generally used in Air craft transportation.



## Necessity of Refrgm.

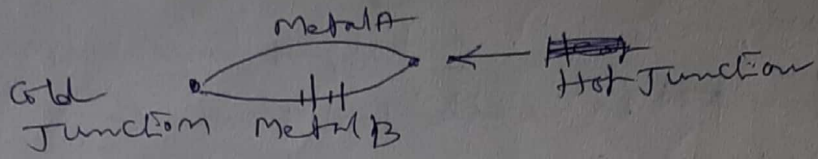
At lower temps, growth of bacteria that spoil the food, retards. Refrigeration helps in preserving the ~~low~~ perishable food products for longer time

## Applications of Refrgm:

- ① Manufacturing of Ice ~~by~~
- ② Preservation of food ~~by~~ by reducing the perishable characteristics.
- 3) Cold storages - To preserve food, vegetables, fruits etc & release to market when required
- 4) Storing of food, making of ice cubes, Keeping the drinking water cool in domestic Refrigerators
- 5) Cooling of water in water coolers, ice cream in deep Freezers etc
- 6) Refrigeration is used in food processing industries, like ice-cream, milk, Cheese etc
- 7) Used in chemical industries, refineries, Paper, pulp industries etc
- 8) Refrigeration & humidity control is useful in Textile industries
- 9) Fruit juices & beverages taste good when served cold. Hence Refrigeration is used
- 10) Refrigeration is used in Comfort Air Conditioning
- 11) For better quality of product & Comfort for workers, industrial A/C is used
- 12) Refrigerated Trucks/vans are used to keep the food/vegetables/fruits during transportation
- 13) For human comfort Refrigeration & A/C principles are used in transportation (A/C buses, A/C Cars, A/C in Aero planes)
- 14) low ~~to~~ Temp Refrgm is used to achieve liquefaction of gases.

Other methods of Refrig

1) Thermoelectric Refrig



Depends on Seebeck & Peltiereffects. when two dissimilar materials are connected as shown in fig and current is passed then cooling is observed at one junction. ~~This principle is used in space vehicles.~~

2) vortex tube refrigeration

Here compressed air <sup>passes</sup> in vortex tube consisting of nozzle <sup>in</sup> diaphragm. Rotational motion is created and hot & cold air streams are separated. Cold air is used for A/C applications & hot air is discharged outside. (nozzle, diaphragm, valve, hot air side, cold air side)

Properties of Air & other principles.

① BT, WBT, RH, Moisture content.

Principles of cooling, heating & dehumidification, heating & humidification.

Heat load calculations in brief.

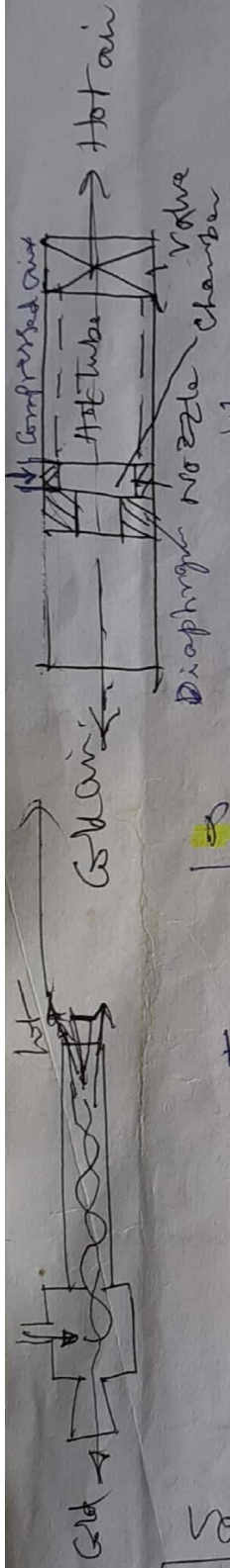
Principles of Sensible heat, latent heat, Total heat. Sensible Heat ratio.

Comfort of human beings.

evaporation causes cooling.

Co-efficient of Performance (C.O.P).

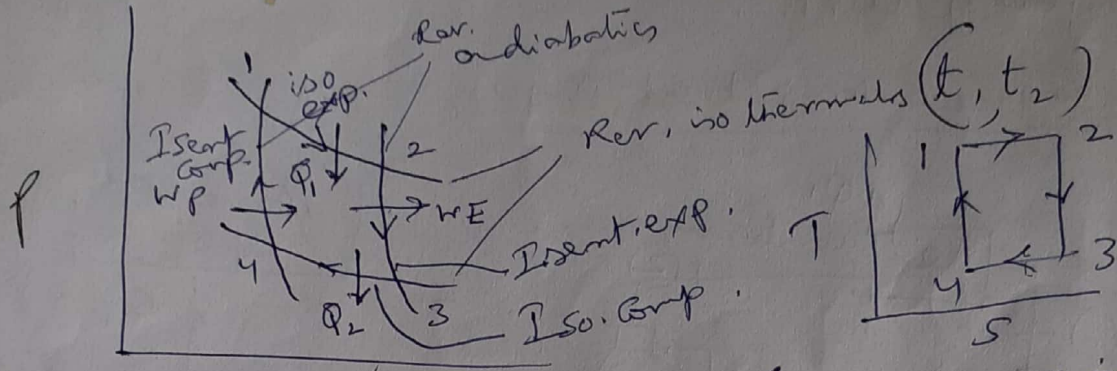
Vortex Tube: chamber is a portion of nozzle. Chambers are gradually converted into spiral form. Valve obstructs the flow of air through hot side & controls the qty of hot air through vortex tube. A stream of air passes through diaphragm hole. Cold goes out from cold side.



Engine, Refrigerator & Heat Pump.

Carnot cycle

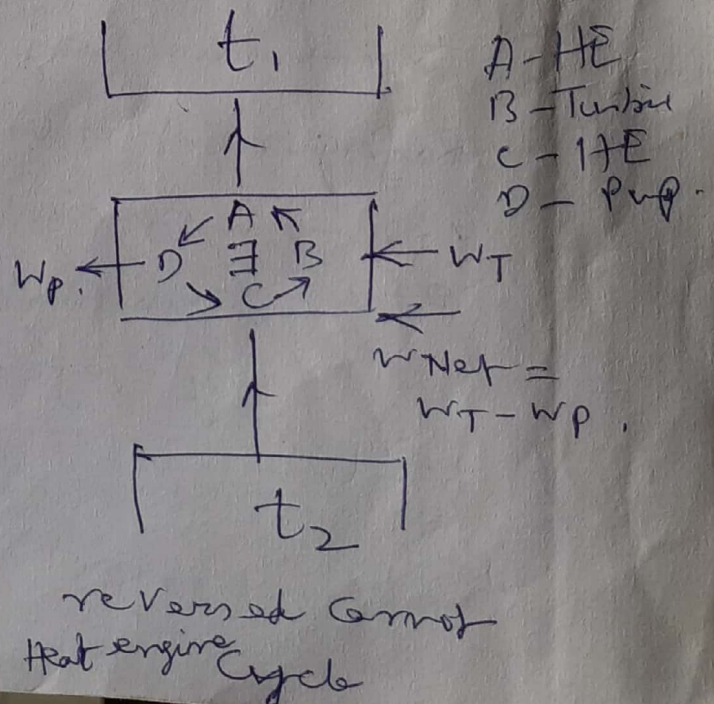
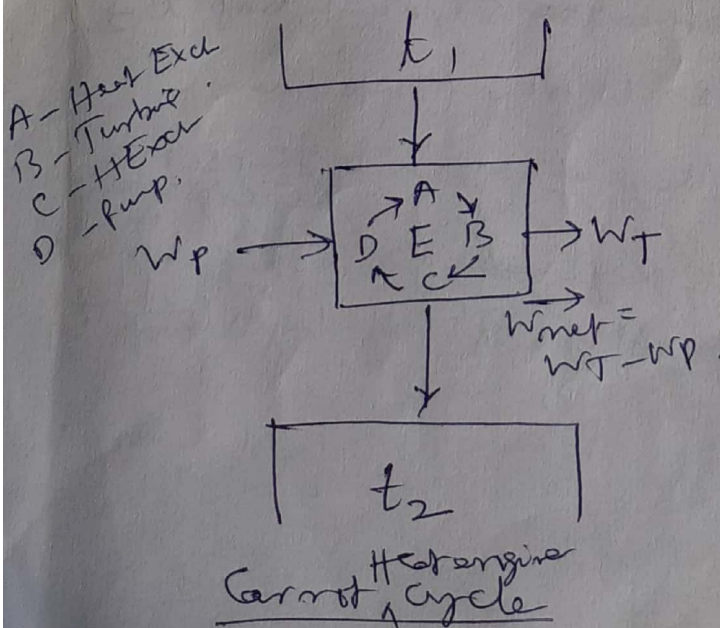
$$\eta = 1 - \frac{T_3}{T_1}$$



- 1) 1-2 → Rev. isothermal process ( $T_1$ ). Heat  $Q_1$  enters. (Reversible)
- 2) 2-3 → Rev. adiabatic →  $W_E$  work is done by system. Temp decreases from  $T_1$  to  $T_2$  ( $W_E$  or  $W_T$ )
- 3) 3-4 → Rev. isothermal process. Heat  $Q_2$  leaves the system at  $T_2$
- 4) 4-1 → Rev. adiabatic process.  $W_P$  is done upon the system. Temp rises from  $T_2$  to  $T_1$ .

Reversed Carnot cycle

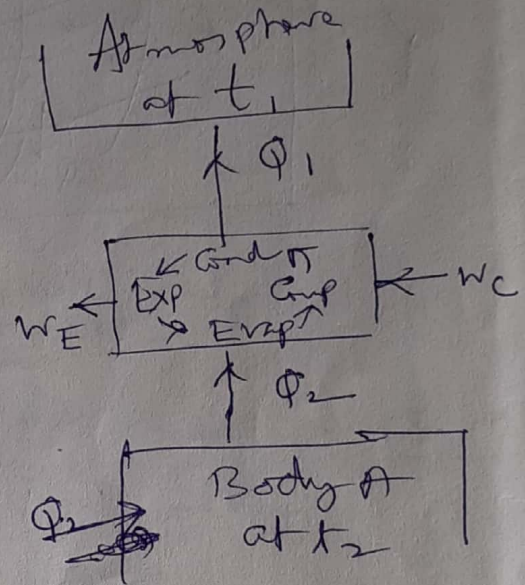
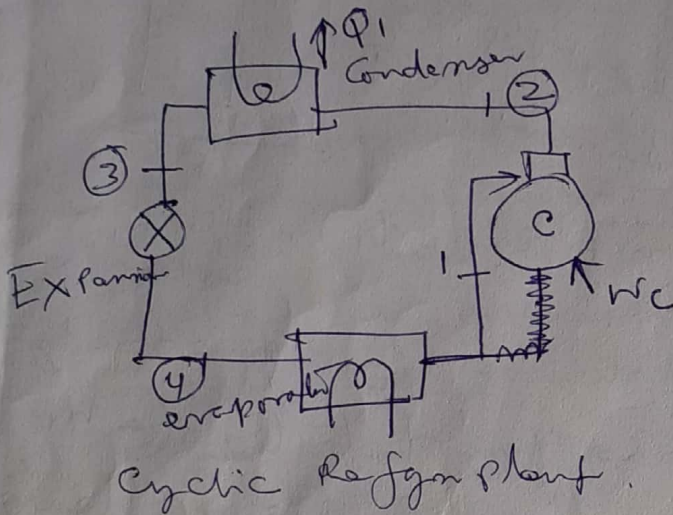
Since all the processes of Carnot cycle are reversible, it is possible to imagine the reversed processes.



Reversed Heat engine

Here heat is taken from low temp body & discharged to high temp body, receives inward flow of work.

Refrigerator & Heat pump



Refrigerator :- maintains a body at a temp

lower than the temp of surroundings. Let body A be maintained at  $t_2$  which is lower than the ambient temp  $t_1$ . Even though A is insulated, heat leakage  $Q_2$  into the ~~body~~ will always be there from surroundings. This  $Q_2$  is to be removed to maintain Body A at a ~~temp~~ constant temp  $t_2$ .

Refrigerant is used as working medium.

- 1-2 -> Compression of Ref vapour. Temp & P increase
- 2-3 -> Condensation of Ref ~~gas~~ gas to ~~liquid~~ liquid by rejection of heat at high temp  $t_1$
- 3-4 ->

The working fluid (Refrigerant) absorbs heat  $Q_2$  at the evaporator (refrigerant takes the heat & latent heat of vapourisation comes into picture, refrigerant becomes a vapour). (Process 4-1)

The Ref vapour is compressed by Compressor ( $C_1$ ) driven by motor which absorbs work ( $W_c$ ) (Process 1-2) Refrigerant becomes hot and press is ~~is~~ raised.

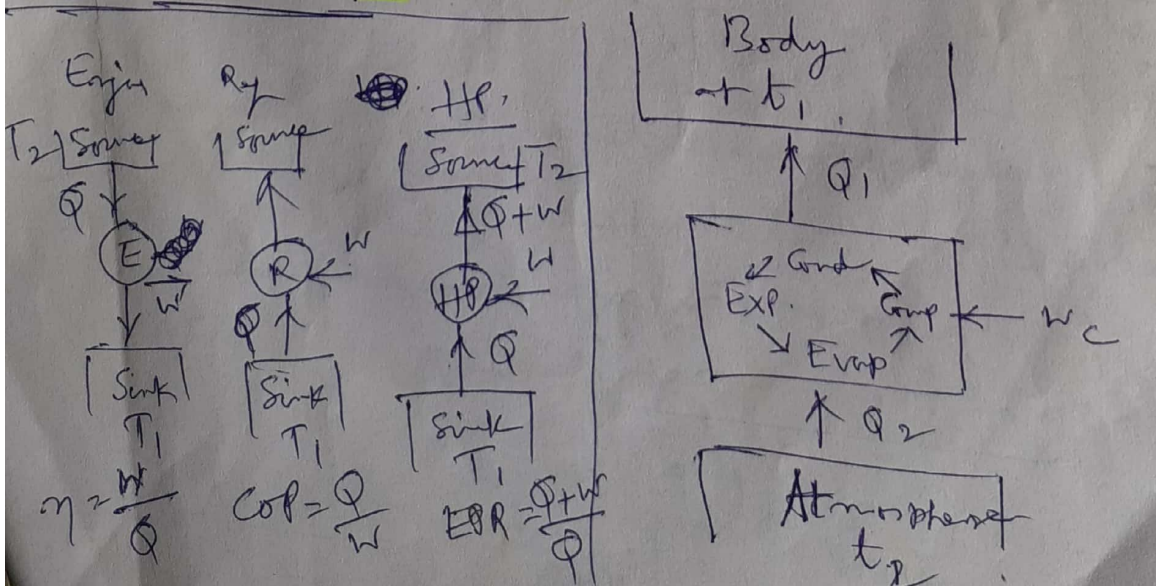
It is sent to condenser (Process 2-3) where heat is rejected (latent heat of condensation) in the condenser to the atmosphere or water coolant at a higher temp  $t_1$ . The refrigerant becomes a liquid but still at high temp. ( $t_1$ ). This condensate expands adiabatically in expansion valve & temp drops to a value lower than  $t_2$ . Cycle repeats. Such a cycle is called Refrigerator.

Co-efficient of performance = C.O.P.

$$C.O.P = \frac{\text{Desired effect or Refgn Effect}}{\text{Work input or work done}}$$

$$= \frac{Q_2}{W_c} = \frac{Q_2}{Q_1 - Q_2}$$

### Heat pump



The principle is useful in winter conditions where Atmospheric temp is low. ~~→~~ & we want maintain comfortable hot temps in the room. Always heat transfer takes place from room to outside and in order to maintain the room temp ~~Heat~~ Heat pump principle is used. It is a simple case of Refrigerator, but evaporator ~~becomes~~ & Condenser are used differently.

Heat is extracted from low Temp reservoir (Atmosphere) & discharged to high Temp body B with expenditure of work (work of compression). The working is similar to Refrigerator. But attention is focussed on high Temp body B.

$$(C.O.P.)_{HP} = \frac{Q_1}{W} = \frac{Q_1}{Q_1 - Q_2}$$

Take ~~out~~

$$1 + \frac{Q_2}{Q_1 - Q_2} = \frac{Q_1 - Q_2 + Q_2}{Q_1 - Q_2} = \frac{Q_1}{Q_1 - Q_2}$$

ie)  $1 + (C.O.P.)_{Ref} = (C.O.P.)_{HP}$

$(C.O.P.)_{HP} > (C.O.P.)_{Ref}$

$$\frac{Q_1}{W} = (C.O.P.)_{HP}, \quad Q_1 = (C.O.P.)_{HP} \times (W)$$

$$Q_1 = [(C.O.P.)_{Ref} + 1] \times (W)$$

$Q_1$  is always greater than  $W$ .

For Electrical resistance heater,  $Q = W$ .

But for Heat pump has got thermodynamic advantage over direct heating.

HE

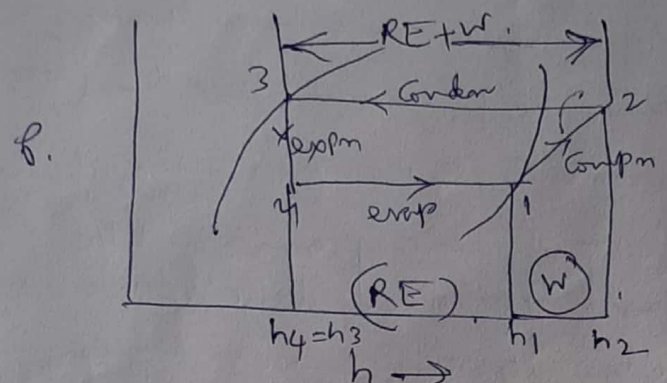
$$\eta_{Carnot HE} = 1 - \frac{Q_c}{Q_H} = 1 - \frac{T_c}{T_H}$$

$$COP_{Carnot HP} = \frac{T_H}{T_H - T_c}, \quad COP_{Carnot R} = \frac{Q_c}{Q_H - Q_c} = \frac{T_c}{T_H - T_c}$$

Relative C.O.P =  $\frac{\text{Actual C.O.P.}}{\text{Theoretical C.O.P.}}$

Performance of heat pump is called Energy Performance ratio (E.P.R)

E.P.R = (C.O.P)<sub>HP</sub>

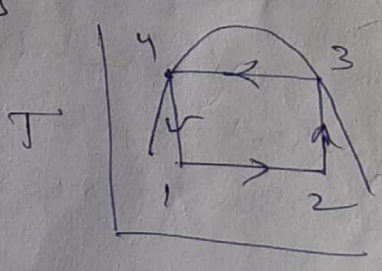
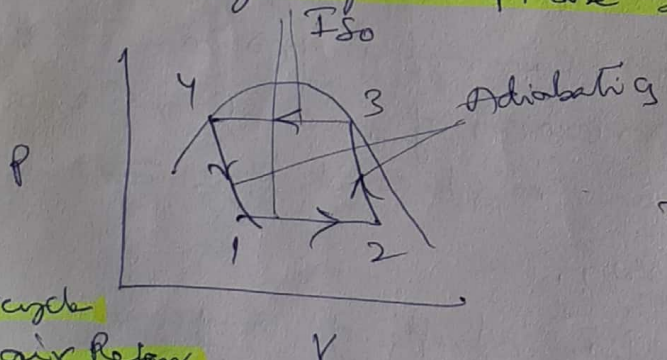


$RE = h_1 - h_4$  ,  $W = h_2 - h_1$

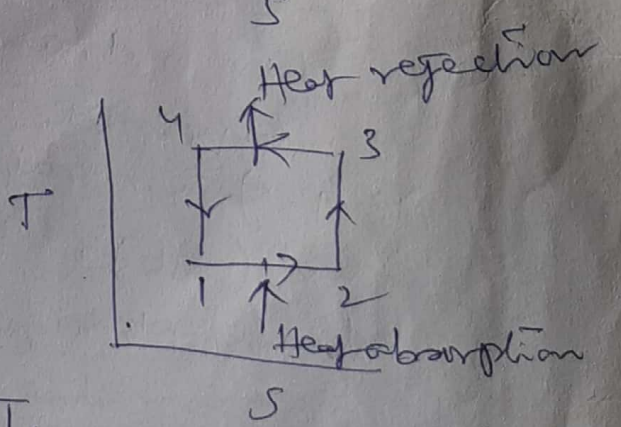
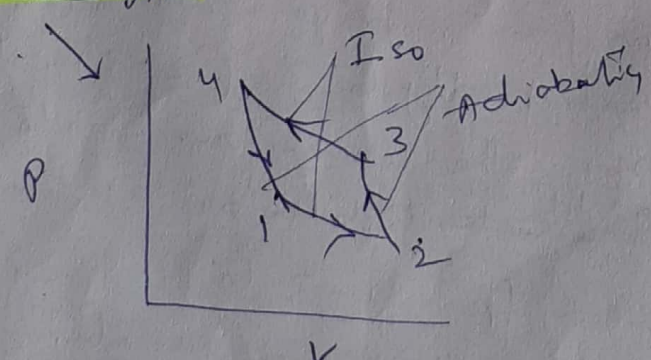
Heat rejection in condenser =  $h_2 - h_3 = (h_2 - h_1) + (h_1 - h_3)$   
 $= RE + \text{Workdone} = h_2 - h_3$

Problems 3.1, 3.2, 3.3, 3.4, 3.6, ~~3.5~~

Carnot cycle for 2 phase systems (vapour refrigerant)



Carnot cycle for air refrigeration



C.O.P =  $\frac{T_1}{T_2 - T_1}$  where  $T_2 > T_1$

## Air Refrigeration System

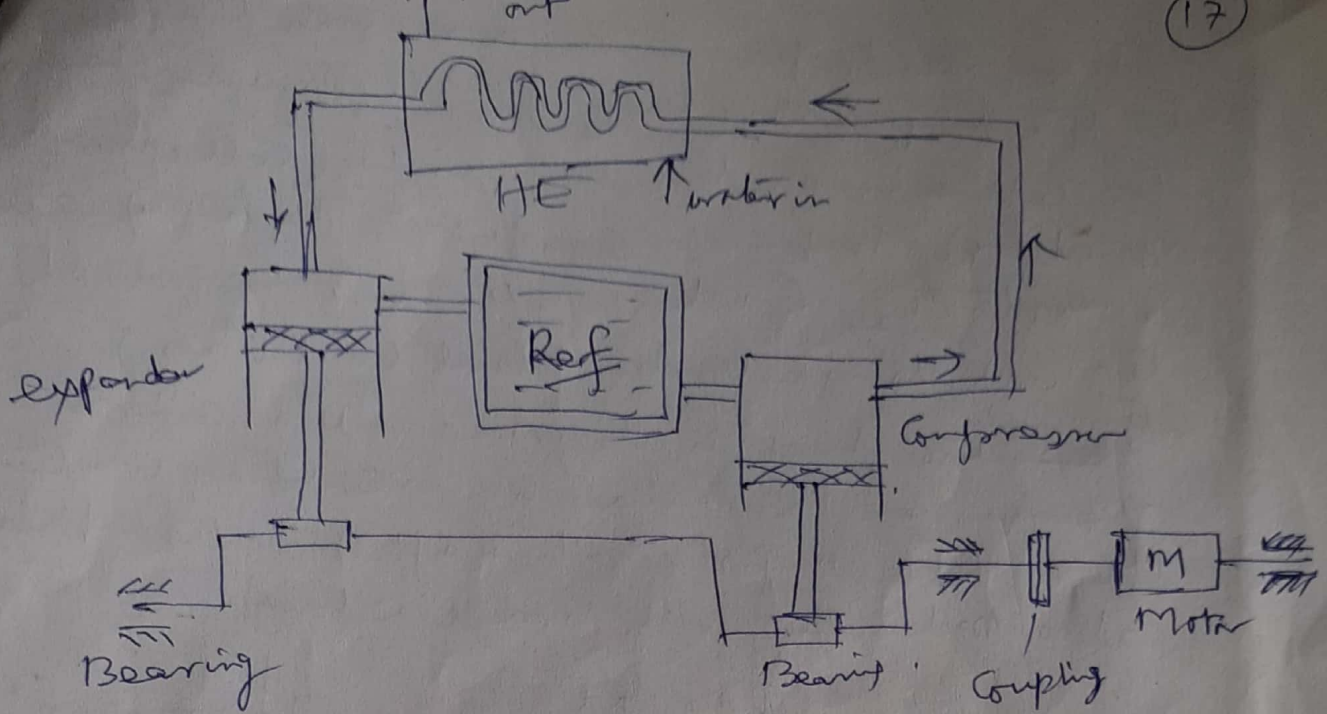
The working fluid is air. Absorbing heat at low temp system & discharging the heat to high temp system is done by air. Air doesn't change the phase through out the system, unlike the vapour compression cycle where there is change of phase for the refrigerant used (ex: Freons,  $\text{NH}_3$ ). Hence the heat carrying capacity per kg of air is small compared to vapour compression cycle. The C.O.P also is less. In olden days it was used. But became obsolete for some years. Again its importance is ~~not~~ recognised in A/C systems of aeroplane. As high pressure <sup>air</sup> is already available in aeroplane, Air refrigeration gained importance in Air craft cooling.

## Bell-Coleman Air Refrigerator

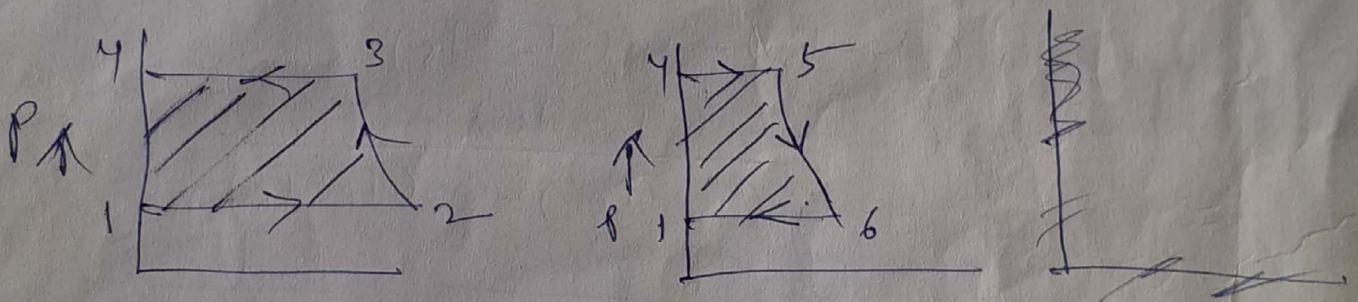
This is one of the earliest refrigeration systems & used in ships carrying frozen meat. The isothermal processes of ideal reversed Carnot cycle are replaced by ~~two~~ constant pressure processes.

1-2  $\rightarrow$  suction stroke of compressor,  
(Air is drawn from refrigerator) ~~and~~  
It is compressed isentropically to 3 (2-3). ~~The~~  
Temp of air raises. The warm air goes to  
cooler (HE). The ~~HE~~ <sup>HE</sup> cools the air at const pr,  
The volume gets reduced from 4-3 to 4-5. & its  
temp  $\rightarrow$  is reduced to that of cooling water in HE.  
The cold air is drawn into expansion cylinder  
during its suction stroke (4-5) & expanded



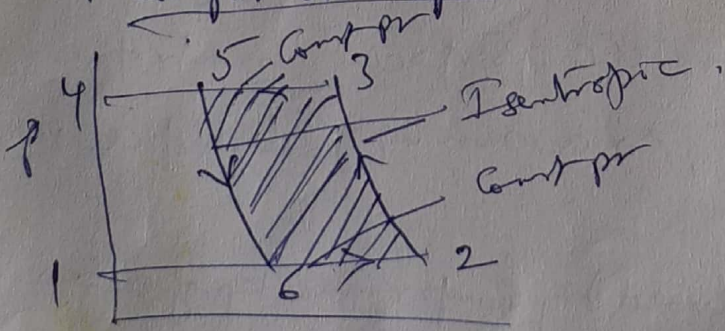


Closed cycle air Refrigerator working on Bell-Goleman cycle.

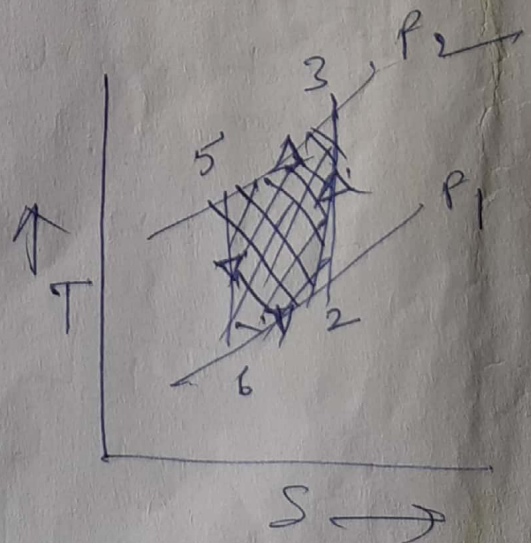


Compressor operation

Expander operation



Bell Goleman cycle



air Refgr in T-S diagram

(18)

The isentropic expansion cools the air to the temp below that of Gold storage chamber. The cold air enters Refrigerator (Gold storage) & absorbs heat at const pr. The temp of air raises to  $T_2$  (which is the temp required in the Gold storage under ideal conditions).  
 In this cycle ~~the~~ the heat is absorbed in the Gold storage chamber and rejected to circulating water in HE. The Refrigerating effect is the heat absorbed in the Gold storage chamber.

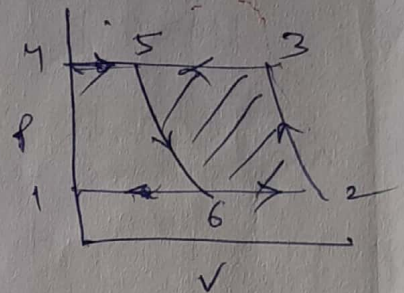
$$C.O.P = \frac{Q}{W} = \frac{RE}{\text{workdone}}$$

$$W = \text{Heat rejected} - \text{Heat absorbed}$$

$$= C_p (T_3 - T_5) - C_p (T_2 - T_6)$$

$$C.O.P = \frac{C_p (T_2 - T_6)}{C_p (T_3 - T_5) - C_p (T_2 - T_6)}$$

$$= \frac{T_2 - T_6}{(T_3 - T_5) - (T_2 - T_6)} = \frac{1}{\frac{T_3 - T_5}{T_2 - T_6} - 1}$$



In actual practice perfect isentropic process is not possible, so assuming polytropic process  $pV^n = C$ .

$W_c$  (work required by comp. per kg of air)

$$= \frac{n}{n-1} [p_3 v_3 - p_2 v_2] = \frac{n}{n-1} R [T_3 - T_2]$$

$W_e$  = work delivered by expander per kg of air

$$= \frac{n}{n-1} [p_5 v_5 - p_6 v_6] = \frac{n}{n-1} R (T_5 - T_6)$$

work delivered by Motor in heat units

$$= W_m = W_c - W_e$$

$$W_m = \frac{n}{n-1} \cdot R [(T_3 - T_2) - (T_5 - T_6)]$$

$C_p - C_v = R$ ,  $\frac{C_p}{C_v} = \gamma$   
 divide by  $C_v$   
 $\frac{C_p}{C_v} - 1 = \frac{R}{C_v}$   
 $\gamma - 1 = \frac{R}{C_v}$   
 $R = C_v (\gamma - 1)$

$C_p - C_v = R$   
 divide by  $C_p$   
 $1 - \frac{1}{\gamma} = \frac{R}{C_p}$   
 $\frac{\gamma - 1}{\gamma} = \frac{R}{C_p}$ ,  $C_p = \frac{R \cdot \gamma}{\gamma - 1}$   
 $R = C_p \left( \frac{\gamma - 1}{\gamma} \right)$

From MKS units  $C_p - C_v = R/5$ , In SI units  $\gamma = 1.4$ .

$$W_m = \left( \frac{n}{n-1} \right) \frac{C_p \left( \frac{\gamma - 1}{\gamma} \right) [(T_3 - T_2) - (T_5 - T_6)]}{1}$$

$$= \left( \frac{n}{n-1} \right) \left( \frac{\gamma - 1}{\gamma} \right) C_p [(T_3 - T_2) - (T_5 - T_6)]$$

C.O.P =  $\frac{Q}{W_m} = \frac{C_p (T_2 - T_6)}{\left( \frac{n}{n-1} \right) \left( \frac{\gamma - 1}{\gamma} \right) C_p [(T_3 - T_2) - (T_5 - T_6)]}$

Divide by  $(T_2 - T_6)$

$$C.O.P = \frac{1}{\left( \frac{n}{n-1} \right) \left( \frac{\gamma - 1}{\gamma} \right) \left[ \frac{T_3 - T_5}{T_2 - T_6} - 1 \right]}$$

As  $T_5 = T_2$  for perfect inter cooling.

For isentropic,  $n = \gamma$ .  
 For ideal isentropic process

$$C.O.P = \frac{1}{\frac{T_3 - T_5}{T_2 - T_6} - 1}$$

$$C.O.P_2 = \frac{T_3}{T_2} \left[ \frac{1 - \frac{T_5}{T_3}}{1 - \frac{T_6}{T_2}} \right] - 1$$

we know that by isentropic law

$$\frac{T_3}{T_2} = \left(\frac{P_2}{P_1}\right)^{\gamma-1/\gamma}$$

$$\frac{T_5}{T_6} = \left(\frac{P_2}{P_1}\right)^{\frac{\gamma-1}{\gamma}}$$

Hence  $\frac{T_3}{T_2} = \frac{T_5}{T_6}$  or  $\frac{T_6}{T_2} = \frac{T_5}{T_3}$

Substituting this

C.O.P. (isentropic process) =

$$\frac{T_3}{T_2} \left[ \frac{1 - \frac{T_6}{T_2}}{1 - \frac{T_6}{T_2}} \right]$$

$$= \frac{1}{\frac{T_3}{T_2} - 1} = \frac{T_2}{T_3 - T_2}$$

C.O.P. (polytropic)

$$= \frac{T_2}{\left(\frac{n}{n-1}\right) \left(\frac{\gamma-1}{\gamma}\right) (T_3 - T_2)}$$

Generally if refrigeration temp =  $T_2$   
 $T_6 < T_2$

For Carnot cycle  $T_6 = T_2$  (ie sink temp is Ref Temp)

In Bell Coleman cycle  $T_3 > T_5$

If Carnot cycle is used,  $T_5 = T_3$  (Source Temp)

$$(C.O.P.)_{Carnot} = \frac{T_2}{T_5 - T_2}$$

we can see that

$$\frac{T_2}{T_5 - T_2} > \frac{T_2}{T_3 - T_2}$$

**(C.O.P.) Carnot > C.O.P. (Bell Coleman)**

Solve for

$$P_2 V_3 = RT_3$$

$$P_1 V_2 = RT_2$$

$$P_2 V_3^{\gamma} = P_1 V_2^{\gamma}$$

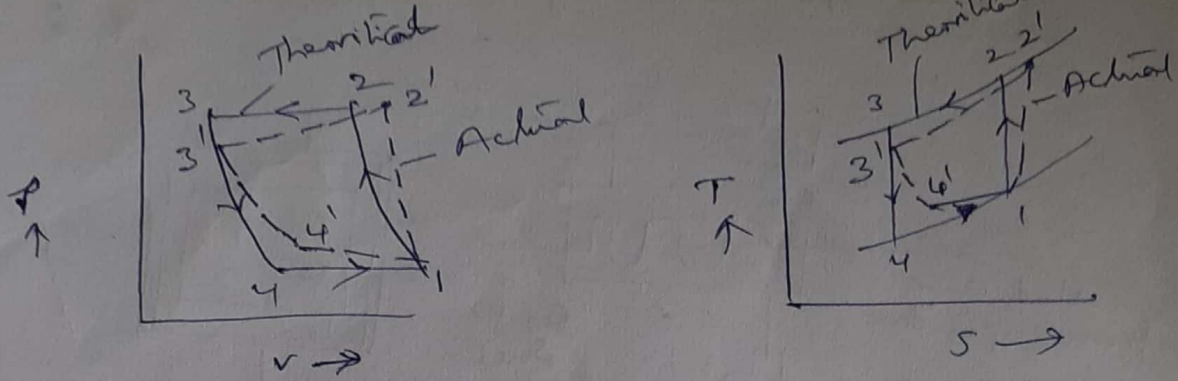
$$\frac{P_2}{P_1} = \left(\frac{V_2}{V_3}\right)^{\gamma}$$

$$= \left(\frac{RT_2 \times P_2}{RT_3}\right)^{1/\gamma}$$

$$\left(\frac{P_2}{P_1}\right)^{\gamma} = \left(\frac{T_2}{T_3}\right)^{\gamma}$$

## Actual analysis of Bell Coleman Cycle.

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Actual cycle differs in following ways

- ① Compn & expn processes doesn't follow isentropic process due to friction, therefore the processes can be considered as irreversible adiabatic (increase in entropy)
- ② Pressure drop takes place in Cooler (HE)
- ③ Pressure drop takes place in Refrigerant also. Hence  $p_r$  at the outlet of expansion is greater than  $p_r$  in Refrigerant. (see fig)

## Advantages & disadvantages of Air Refgn system

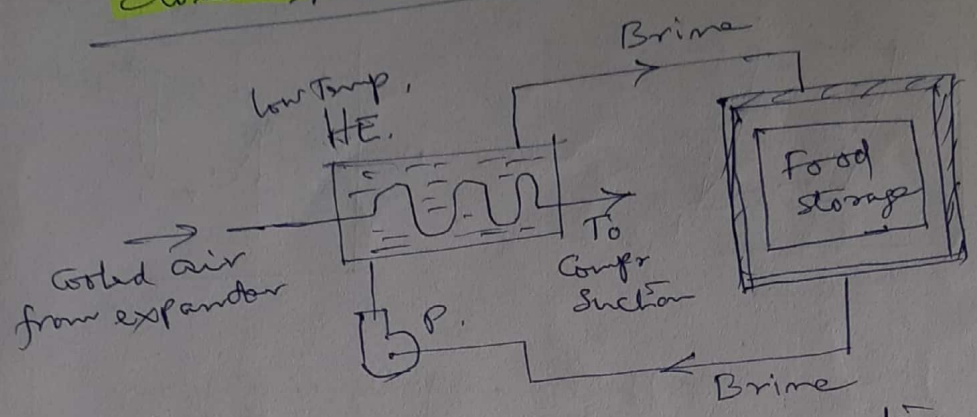
### Advantages:

- ① Air is easily available & cheap.
- ② Air is non-inflammable. So <sup>no</sup> danger of fire
- ③ Weight of air refgn system is lower than that of other refgn systems. Hence preferred in Aircraft ~~ref~~ refrigeration.

### Disadvantages

- ① Heat is carried by air in the form of sensible heat only, hence weight of air to be circulated is more than other refrigerants
- ② C.O.P of system is low
- ③ Major disadvantage of ~~this~~ <sup>this</sup> system is freezing of moisture in the air. formation of snow choke the valves. This is overcome in closed system.

Closed type air refg system



Here cold air gets the brine & this brine is sent to refrigerated space to cool the products. This process is known as closed system. In open system cold air is sent directly to the refrigerated space. In closed system air doesn't come into direct contact with food items. (Fruits, vegetables etc) Hence air can be kept nearly dry in this case, whereas in open system air cannot be kept dry, hence frost formation will be there when low temperatures are used.

Air craft Refrigeration systems  
Necessity of cooling the Aeroplane.

There are many external & internal heat sources in Aeroplane. Hence A/C is required. (2°C for comfort, -5°C for food preservation).  
Major heat sources.

- ① External (1) Heat from Sun
- (2) Pressure of the atmosphere reduces at high altitudes. But Cabin pr should be maintained at Atmospheric pr. ~~As the~~ ~~pressure~~ Hence compressed air is used for Cabin. It will be hot, ~~so refg is~~ so A/C is ~~not~~ required.

③ Because of fast movement of plane, ~~it is~~ skin friction occurs all over the air craft with air. Hence heat flows into the ~~air~~ cabin.  
 (Ex An Aero plane moving at 1000 km/hr, will experience 5°C rise in temp of the surface.)

Internal Sources

- ① Human beings generate heat (400 KJ/hr approx at rest)
  - ② Electrical, electronic equipment generate heat.
  - ③ engine ~~parts~~ parts get heated up. & heat is passed to cabin.
- Hence A/C is required

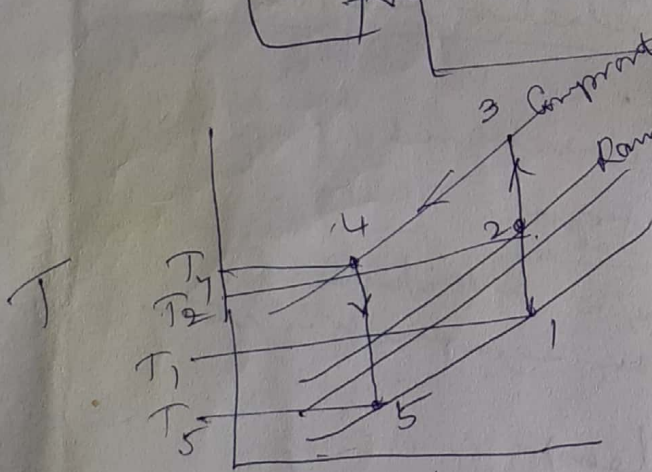
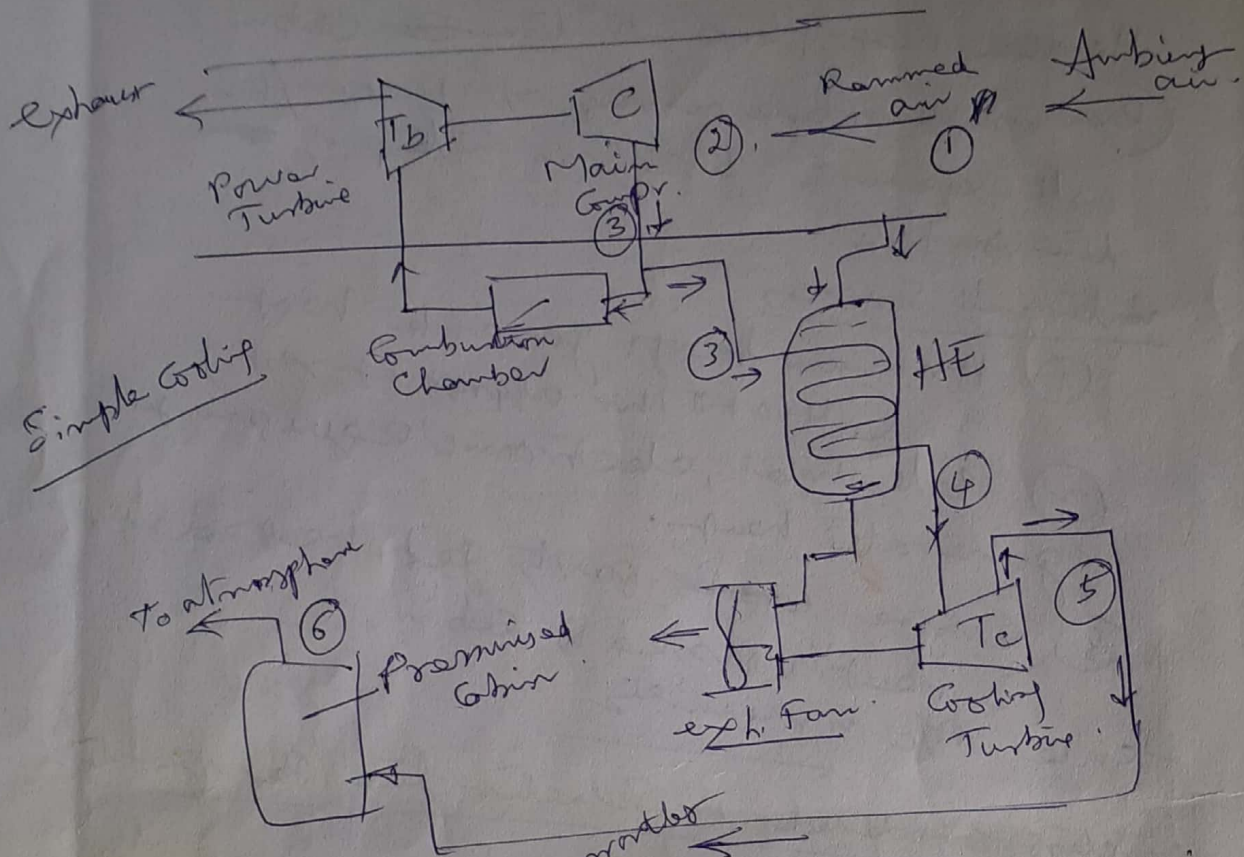
Factors considered in selecting the Refrigeration system for Aero plane.

Air cycle refrigeration is preferred.

Advantages of Air Refrig

- 1) As compressed air is available, separate compression equipment is not required
- 2) weight/TR is least
- 3) space & volume required is less
- 4) Air is non-inflammable
- 5) leakage problems with Air refri is less
- 6) Maintenance ~~cost~~ <sup>Cost</sup> is low.
- 7) repairs are easy,

Simple cooling with simple Evaporative Type Aeroplane Air conditioning



- 1-2 ramming
- 2-3 Compression in Main Comp.
- 3-4 - Cooling in HE
- 4-5 - Expan in C.T.
- 5-6 - Heat gain

Qty of air taken for Ref purpose

$$m_a = \frac{3.5 T}{C_p (T_6 - T_5)}$$

Cooling load =  $T$   
Temp of Ref

Power required kW =  $m_a \cdot C_p \cdot (T_3 - T_2)$

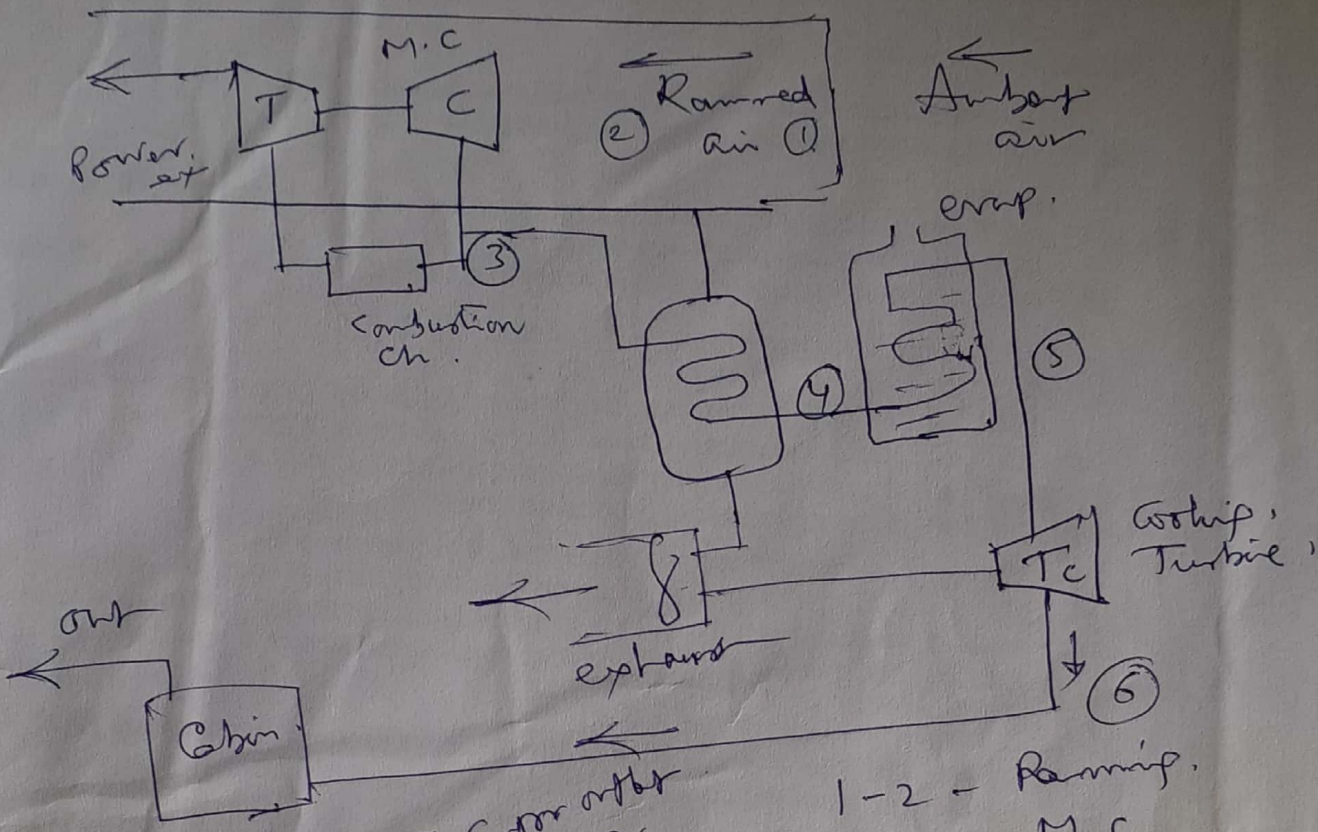
$$C.O.P = \frac{3.5 T}{KW}$$

$m_a$  = Mass of air per sec  
 $C_p$  = Sp. ht.  $T = TR$

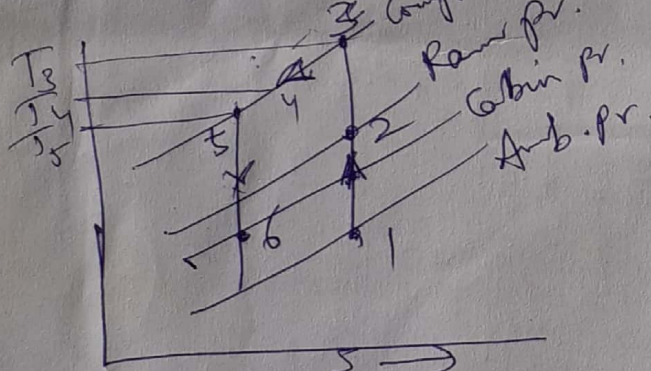


Simple evaporative Type

Simple evaporative Cooling System



- 1-2 - Ramming.
- 2-3 - M.C
- 3-4 - Cooling in HE
- 4-5 - " " evap.
- 5-6 - Cooling Turbine.



~~water~~, Methyl alcohol,  $NH_3$  all have been used in evap.

Mass of liq to be carried

$m = \text{Mass of } \text{evaporant carried}$

$Q = \text{Heat removed in evap.}$

$t = \text{Flight time in minutes}$

$h_{fg} = \text{L.H of evaporant in kJ/kg}$

$$m = \frac{Q \cdot t}{h_{fg}}$$

# Boot strap & Boot strap evaporative Type

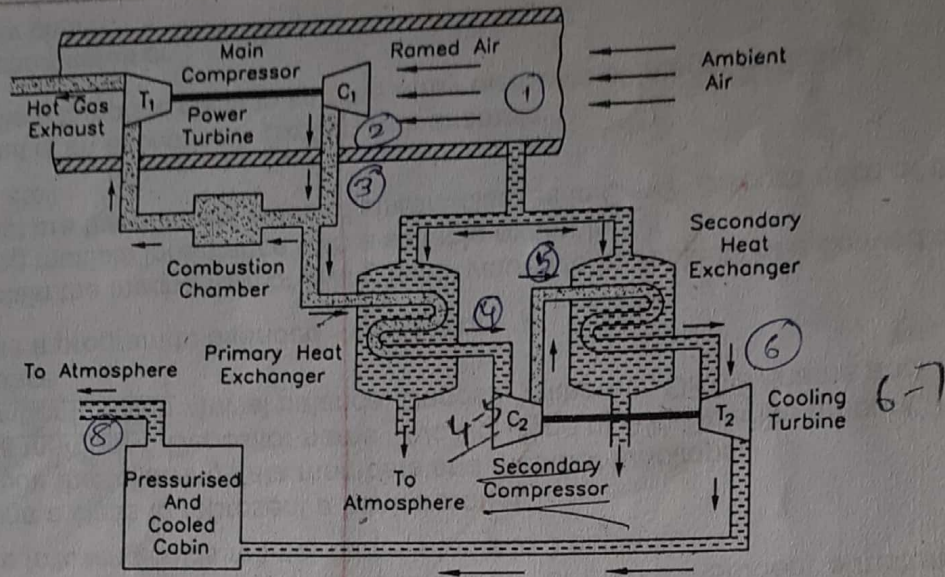


Fig. 3.13. (a) Boot-Strap air-cycle Refrigeration System.

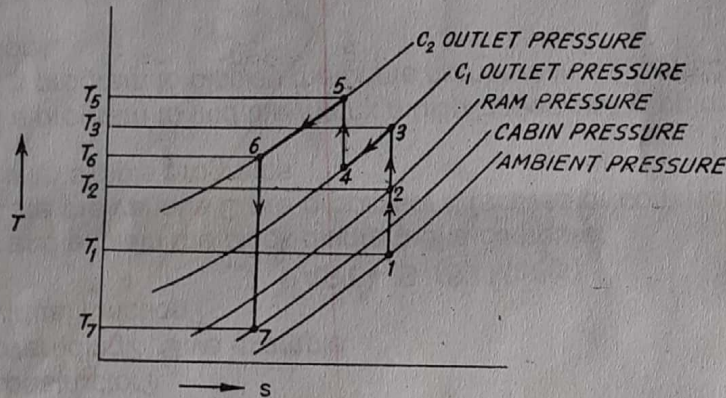


Fig. 3.13. (b) Representation of boot-strap cooling system on  $T-s$  diagram.

- 1 - 2 → Ramming action.
- 2 - 3 → Compression in main compressor  $C_1$ .
- 3 - 4 → Cooling in the primary heat exchanger.
- 4 - 5 → Compression in secondary compressor  $C_2$ .
- 5 - 6 → Cooling in the secondary heat exchanger.
- 6 - 7 → Expansion in the cooling turbine.

is first cooled in the primary heat exchanger. The air is then compressed to a higher pressure in the secondary compressor. It is further cooled in the secondary heat exchanger and further cooling action is completed by expanding the air through cooling turbine. Ram air is used as a heat sink in the primary and

Here the pressure of working fluid is raised to a higher level than the ~~MC~~ M.C. (Main Compressor) by a separate comp before expansion. The power required for the sec. comp is taken from the Cooling Turbine.

Bootstrap air cycle refrigeration system is used most frequently in transport type aircraft.

Cooling load is  $T$  Tons

Quantity of air circulated  $=$   
 $= m_a = \frac{3.5 T}{C_p (T_8 - T_7)}$

where  $T_8$  is the temp of air leaving the cabin.

Power reqd  $= kW = m_a \cdot C_p \cdot (T_3 - T_2)$

work reqd for sec comp is delivered by cooling turbine. So no extra work is reqd.

C.O.P  $= \frac{3.5 T}{m_a \cdot C_p (T_3 - T_2)}$

Bootstrap evaporative

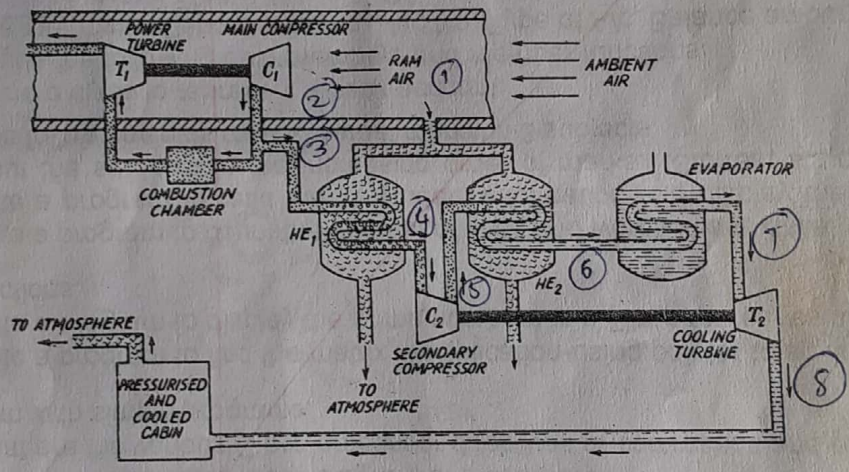


Fig. 3.14 (a). Bootstrap evaporative cooling system.

cooler is located in the high pressure air duct between the secondary heat exchange and cooling turbine. Any suitable evaporant may be used as a heat sink for the evaporative cooler.

- 1 - 2 → Ramming action.
- 2 - 3 → Compression in main compressor.
- 3 - 4 → Cooling in the primary heat exchanger.
- 4 - 5 → Compression in the secondary compressor.
- 5 - 6 → Cooling in the secondary heat exchanger.
- 6 - 7 → Cooling in the evaporator.
- 7 - 8 → Expansion in the cooling turbine.

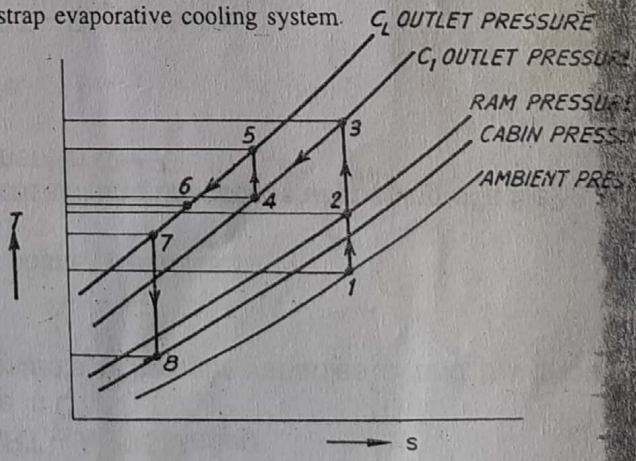


Fig. 3.14 (b). Representation of bootstrap evaporative cooling system on T-s diagram.

The mass of air required in evaporative bootstrap system for taking  $T$  tons of load will be the mass of air required in the bootstrap system as outlet temperature of cooling turbine in evaporative system.

$T_9 =$  outlet temp of Cabin Air.  
 The eqns are similar.

$T_7 =$  Temp of air going out of Cabin.

$$\dot{m}_1 = \frac{3.5T}{c_p(T_7 - T_6)} \text{ kg/sec}$$

$m =$  Total Mass from Main Compressor.

$m_2 =$  Mass used for regenerative HE.

$$m_2 (T_8 - T_6) = m (T_4 - T_5)$$

$$m_2 = \frac{m (T_4 - T_5)}{(T_8 - T_6)}$$

$$KW = m \cdot c_p \cdot (T_3 - T_2)$$

$$C.O.P = \frac{3.5T}{m \cdot c_p (T_3 - T_2)}$$

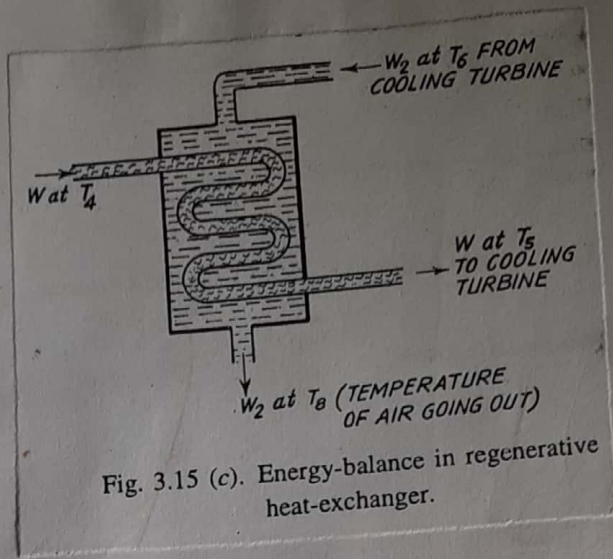


Fig. 3.15 (c). Energy-balance in regenerative heat-exchanger.

### Reduced Ambient Type

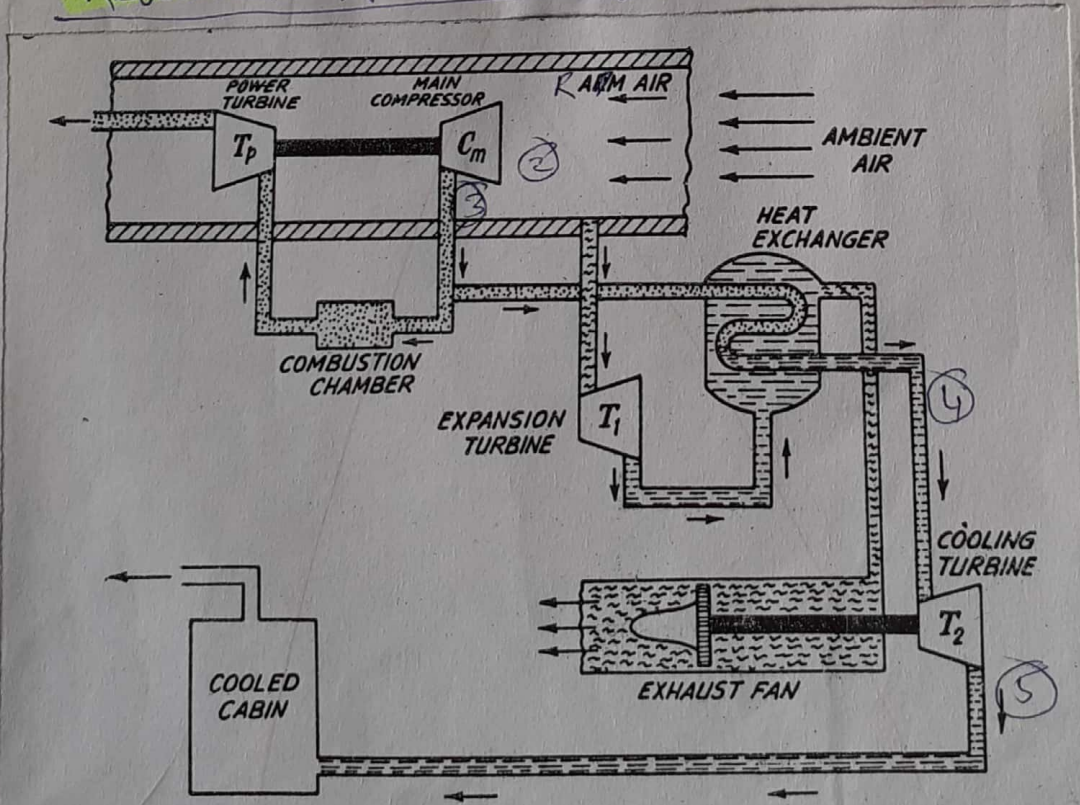
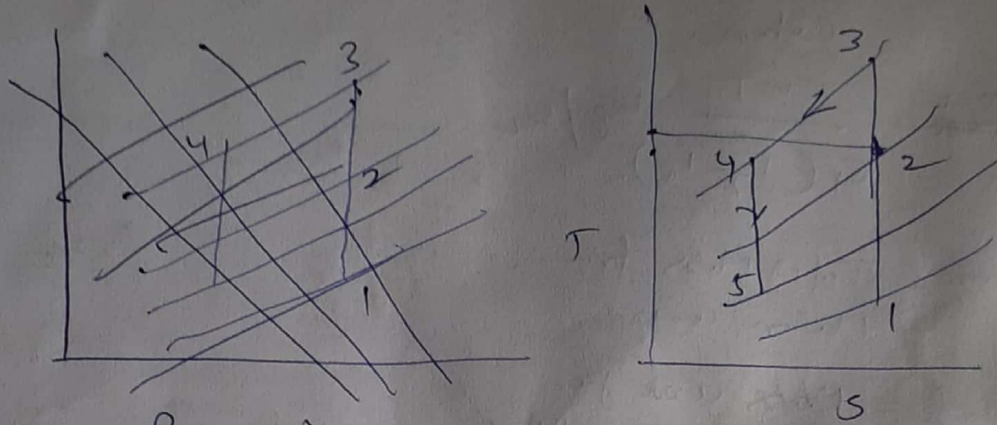


Fig. 3.16 (a) Reduced ambient type cooling system.

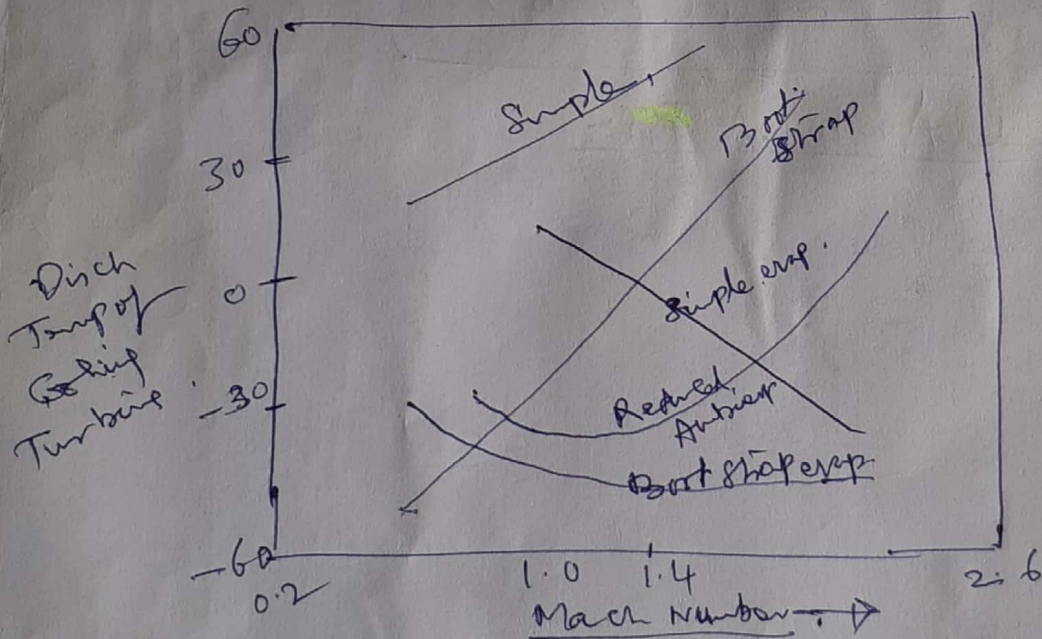
- 1 air to air HE.
- 2 Nos of expansion turbines.



- 1-2 - Ramming
- 2-3 - Compression in M.C.
- 3-4 - HE
- 4-5 - Cooling turbine

Air used for cooling is taken from Turbine T<sub>1</sub>.

Comparison of diff Air Cooling systems used for Air craft.



High Speed. Causes high disch Temp from ~~cooling~~ Turbine.  
 Simple cooling is not effective at high speeds.  
 evaporative bort strap & regenerative system  
 give lower disch Temps. (So adopted for high speed aircraft)

Actual ~~to~~ Air craft A/c with controls

AIR-REFRIGERATION SYSTEMS

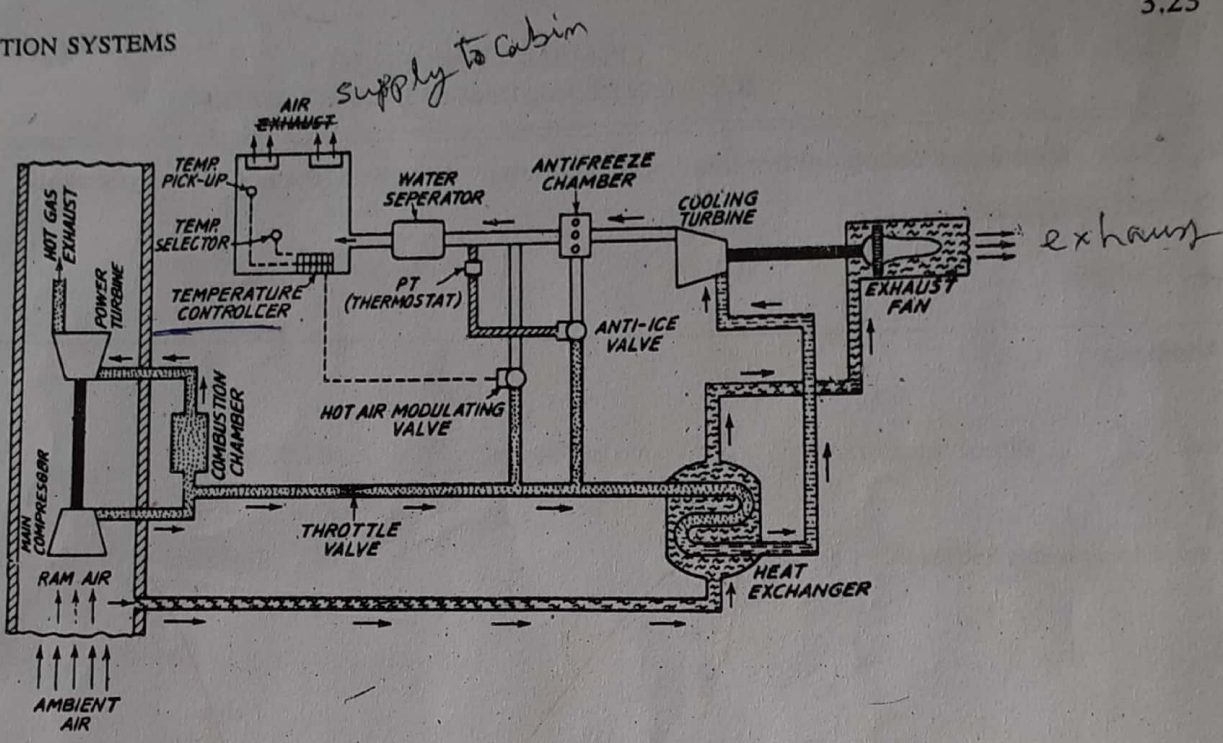


Fig. 3.22. Air conditioning system of aeroplane with controls.

Main Controls

- ① Temp control in Cabin .
- ② Air flow ( Quantity ) control in Cabin .
- ③ Water ~~control~~ separator & anti ice control .

Problems

— X —

Any substance capable of absorbing heat from another substance can be used as refrigerant.

Ex: ice, water, air, brine etc

Generally heat is extracted from lower temp body & dissipated to higher temp body either in the form

Sensible heat (as the case of air refgn) & ~~in the~~ in the form of latent heat (vapour refgn)

Vapour refgn systems are more efficient.

Physical properties, pressures of refgnts must be convenient for operation of equipment.

While selecting, thermodynamic, chemical & safety characteristics of refgnts must be considered.

Air, NH<sub>3</sub>, CO<sub>2</sub>, SO<sub>2</sub>, Methyl chloride were used as refrigerants; till Freons are developed.

Classification:

- ① Primary Refgnts - Directly take part in the refgn system.
- ② Secondary Refgnts - Primary refgnt gets secondary refgnt first & then secondary refgnt gets the product.

Primary refgnts

① Halo carbon compounds.

Ethane, Methane react with halogens (Cl, Br, F) to get compounds.

Refrigerant	Chemical formula	
R-11	Trichloro mono fluoro methane	CCl <sub>3</sub> F
R-12	Dichloro Difluoro methane	CCl <sub>2</sub> F <sub>2</sub>
R-22	Mono chloro Difluoro "	CHClF <sub>2</sub>
R-134a	Tetrafluoro ethane	CH <sub>2</sub> FCF <sub>3</sub>

② Azeotropes:

Mixture of diff refgnts which do not separate out during the process.

Ex. R-500, 73.8% F-12, 26.2% F-152

③ Hydro Carbons:

Satisfactory thermodynamic properties but are highly flammable.  
 R-10 Methane  $C_1H_4$ , ethane  $C_2H_6$   
 R-290 propane  $C_3H_8$ .

④ Inorganic Compounds.

R-717 - Ammonia  $NH_3$  - ice plants  
~~R-10~~ - water (steam jet refriger)  
~~R-22~~ - Air,  $CO_2$ ,  $SO_2$   
 Aircraft (ships)

⑤ Unsaturated Organic Compounds

ethylene  $C_2H_4$   
 propylene  $C_3H_6$  etc

Desirable properties of ideal refrigerants

① Thermodynamic properties.

1) Boiling pt - low boiling pt is reqd.

Refrigerant	B.P. at Atmospheric pr.
Ammonia	-33.3°C
R-12	-29.8°C
R-22	-41.3°C etc

② Freezing pt. low freezing pt reqd.

Refrigerant	F.P.
$NH_3$	-77.8°C
R-12	-157.8
R-22	-160.

③ Evaporator & Condenser pressures:

±ve pressures in evaporator & condenser are desirable. Too high pressures require robust designs (More cost)  
 ±ve pr ~~in~~ in evaporator is required to prevent leakage of air & moisture



Refrigerant	$P_r$ in evaporator -15°C	$P_r$ in condenser at 29°C	Pressure ratio
NH <sub>3</sub>	2.34 bar	11.5 bar	4.92
F-12	1.8 bar	7.32 bar	4.07

Reciprocating compressors are used for refrigerants having low specific volume. ex NH<sub>3</sub>, F12, F22

Centrifugal compressors are used for refrigerants operating under low condensing & condenser pressures.

④ Critical Temp, Critical Pr:

Critical temp of vapour is defined as a temp above which vapour cannot be condensed irrespective of any high pressure. The critical temp of the refrigerant used should be higher than the condensing press for easy condensation.

Ref.	Critical Temp °C	$\frac{C_H d F_2}{m=1, n=1}$	$R_{(n-1)(m+1)q}$
NH <sub>3</sub>	132.8	$p=1, q=2$	$R_{22}$
R-12	112.1	$m+p+q=2(m+1)$	
R-22	95.4	$(1+1+2)=2(m+1)$ $4=4$	

⑤ latent heat of Ref: High latent heat of refrigerant at ~~evap~~ evap temp is desirable for high refrigerating effect. If LH is high, weight of refrigerant circulated is low.

Nomenclature: C<sub>m</sub> H<sub>n</sub> Cl<sub>p</sub> F<sub>q</sub> methyle, ethane base P.T. 0

$(m+p+q=2m+2), R_{(m-1)(m+1)q}$

$C_2 H_2 F_4, m=2, n=0, p=2, q=4$   
 $m+p+q=2(m+1),$  Designation  $R_{(2-1)(0+1)4}$   
 $6=6$   $= R_{114}$

(B) Safe working properties:-

They include

- a) Chemically inert.
- b) non-flammable, non explosive, non toxic
- c) Should not react with lubricating oil.  
(It should be miscible with lub oil)
- d) Leaked refrigerant should not have bad effect on the stored materials

1. Toxicity: Toxic nature of the refigat will effect the human beings when leaked. It causes suffocation, breathing problems & death. It is a major consideration in direct expansion systems.  
 \* Refrigerants non toxic also become toxic when mixed with air in certain percentage.

2. flammability: Most of the refrigerants are non flammable, so danger of explosion doesn't exist.  $NH_3$  &  $CH_2Cl$  burn in air when present in certain concentrations. Methane, ethane, propane are highly flammable.

3. Corrosive Property: Refgat must be non Corrosive

4. Chemically stable :- Should not decompose at normal temp encountered

5. Effect on stored product :- Should not affect quality (Colour, taste)

Physical properties

- 1) sp. vol: low sp. vol at suction to Compr is desirable
- 2) sp. ht: low spht of liq, high spht of vap "
- 3) Thermal conductivity: High conductivities "
- 4) Viscosity: low viscosities are "

Ozone depletion  
 Global warming  
 Alternative Refrigerants